In situ poly(urea-formaldehyde) microencapsulation of dicyclopentadiene

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Microencapsulated healing agents that possess adequate strength, long shelf-life and excellent bonding to the host material are required for self-healing materials. Urea-formaldehyde microcapsules containing dicyclopentadiene were prepared by *in situ* polymerization in an oil-in-water emulsion that meet these requirements for self-healing epoxy. Microcapsules of $10-1000 \,\mu\text{m}$ in diameter were produced by appropriate selection of agitation rate in the range of $200-2000 \,\text{rpm}$. A linear relation exists between log(mean diameter) and log(agitation rate). Surface morphology and shell wall thickness were investigated by optical and electron microscopy. Microcapsules are composed of a smooth $160-220 \,\text{nm}$ inner membrane and a rough, porous outer surface of agglomerated urea-formaldehyde nanoparticles. Surface morphology is influenced by pH of the reacting emulsion and interfacial surface area at the corewater interface. High yields (80-90%) of a free flowing powder of spherical microcapsules were produced with a fill content of $83-92 \,\text{wt}\%$ as determined by CHN analysis.

Keywords: Microcapsule, self-healing, dicyclopentadiene, urea formaldehyde, *in situ* polymerization, surface morphology.

Introduction

Self-healing polymers and composites with microencapsulated healing agents offer tremendous potential for providing long-lived structural materials (White *et al.* 2001). The microcapsules in self-healing polymers not only store the healing agent during quiescent states, but provide a mechanical trigger for the self-healing process when damage occurs in the host material and the capsules rupture. The key feature of self-healing materials is the highly engineered microencapsulated healing agent. The microcapsules must possess sufficient strength to remain intact during processing of the host polymer, yet rupture when the polymer is damaged. High bond strength to the host polymer combined with a moderate strength microcapsule shell are required. To provide long shelf-life the capsules must be impervious to leakage and diffusion of the encapsulated (liquid) healing agent for

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Figure 1. Microencapsulation of DCPD utilizing acid-catalyzed *in situ* polymerization of urea with formaldehyde to form capsule wall.

considerable time. These combined characteristics are achieved with a system based on the *in situ* polymerization of urea-formaldehyde (UF) microcapsules encapsulating dicyclopentadiene (DCPD) healing agent, outlined in figure 1. The addition of these microcapsules to an epoxy matrix also provides a unique toughening mechanism for the composite system (Brown *et al.* 2002).

This paper reports on the manufacture of UF microcapsules prepared by *in situ* polymerization in an oil-in-water emulsion. A basic review of the *in situ* encapsulation technique has been provided by Baxter (1974), Thies (1987, 1996) and Arshady and George (1993). *In situ* encapsulation of water-immiscible liquids by the reaction of urea with formaldehyde at acid pH is outlined by Dietrich *et al.* (1989). Tan *et al.* (1991), Yan *et al.* (1993), Alexandridou and Kiparissides (1994) and Ovez *et al.* (1997) have all shown that microcapsule size can be controlled by adjusting the agitation rate during microencapsulation.

UF microcapsule diameter and surface morphology significantly influence capsule rupture behaviour and healing agent release in self-healing polymers (White *et al.* 2001, Brown *et al.* 2002). In this paper, UF encapsulated DCPD with average diameters ranging from $10-1000 \,\mu\text{m}$ are analysed and the influence of process variables on the capsule surface morphology is described.

Materials and methods

Materials

Dicyclopentadiene was obtained from Acros Organics (Geel, Belgium) and purified by filtration and vacuum distillation prior to microencapsulation. Urea, ammonium chloride and formaldehyde were purchased from Fisher Chemicals (Loughborough, UK). Resorcinol was obtained from J. T. Baker (Phillipsburg, New Jersey). Ethylene maleic anhydride (EMA) copolymer was purchased from Zeeland Chemicals (Zeeland, Michigan). All solvents and substances used for preparation of EMA solution, acid and base solutions and 1-octanol were of analytical grade.

Preparation of microcapsules

Microcapsules were prepared by *in situ* polymerization in an oil-in-water emulsion. At room temperature (20–24°C), 200 ml of deionized water and 50 ml of 2.5 wt% aqueous solution of EMA copolymer were mixed in a 1000 ml beaker. The beaker was suspended in a temperature-controlled water bath on a programmable hotplate with external temperature probe (Dataplate[®] Digital Hotplate, Cole Palmer). The solution was agitated with a digital mixer (Eurostar, IKA Labortechnik) driving a three-bladed, 63.5 mm diameter low-shear mixing propeller (Cole Parmer) placed just above the bottom of the beaker.

Under agitation, 5.00 g urea, 0.50 g ammonium chloride and 0.50 g resorcinol were dissolved in the solution. The pH was raised from ~2.60 to 3.50 by drop-wise addition of sodium hydroxide (NaOH) and hydrochloric acid (HCl). One to two drops of 1-octanol were added to eliminate surface bubbles. A slow stream of 60 ml of DCPD was added to form an emulsion and allowed to stabilize for 10 min. After stabilization, 12.67 g of 37 wt% aqueous solution of formaldehyde was added to obtain a 1:1.9 molar ratio of formaldehyde to urea (Sanghvi and Nairn 1992). The emulsion was covered and heated at a rate of $1^{\circ}C \min^{-1}$ to the target temperature of 55°C. After 4 h of continuous agitation the mixer and hot plate were switched off. Once cooled to ambient temperature, the suspension of microcapsules was separated under vacuum with a coarse-fritted filter. The microcapsules were rinsed with deionized water and air dried for 24–48 h. A sieve was used to aid in separation of the microcapsules (USA standard testing sieves, W. S. Tyler).

Microcapsule size analysis

Microcapsule size analysis was performed with an optical microscope (Optiphot 150S, Nikon) and image analysis software (Global Lab Image V. 3.1, Data Translation). Mean diameter and standard deviation were determined from data sets of at least 250 measurements. The size distribution was biased toward small microcapsule diameters as discussed by Ovez *et al.* (1997). However, the mean and standard deviation captured the dominant mode of the distribution.

Electron microscopy

Surface morphology and capsule shell thickness were examined by scanning electron microscopy (XL30 ESEM-FEG, Philips). Microcapsules were mounted on a conductive stage and ruptured with a razor blade to facilitate membrane thickness measurement. Samples were sputtered with a thin layer (~ 10 nm) of gold-palladium to prevent charging under the electron beam.

Elemental analysis

Microcapsule fill content was measured by elemental analysis using a Carbon-Hydrogen-Nitrogen (CHN) analyser (CE440, Exeter Analytical Inc.). Microcapsule samples combusted at 980°C in an oxygen atmosphere to form CO₂, H₂O and N_xO_y. Knowing the chemical compositions of UF (C₅H₈N₂O, 53.56 wt% C and 24.98 wt% N) and DCPD (C₁₀H₁₂, 90.85 wt% C and 0 wt% N) and assuming that water was the only impurity present in the combusted sample, the weight fractions of UF and DCPD were calculated as

$$w_{\rm UF} = 4.003 \, w_{\rm N}$$
$$w_{\rm DCPD} = 1.101 \, w_{\rm C} - 2.144 \, w_{\rm N} \tag{1}$$

where $w_{\rm C}$ and $w_{\rm N}$ are the weight fractions of C and N obtained by elemental analysis.

Results and discussion

The processing route described in figure 1 produces high quality UF microcapsules with a DCPD core over a wide range of sizes for use in self-healing structural polymers and polymer composites. The microcapsules are spherical and free flowing after drying (see figure 2). Yields of the preparation, defined by the ratio of the mass of recovered microcapsules to the total mass of DCPD core and shell constituents, are high. At 550 rpm agitation rate, the typical yield is 79–92%. Fracture of microcapsules under high shear conditions and non-recoverable microcapsule build-up on the reaction beaker result in lower yields as agitation rate increases. At 1800 rpm agitation rate, the typical yield is greater than 68%.

Control of diameter

Average microcapsule diameter is controlled by agitation rate, as shown in figure 3. As the agitation rate is increased, a finer emulsion is obtained and the average microcapsule diameter decreases. Microcapsules with average diameter in the range of $10-1000 \,\mu\text{m}$ are obtained by adjusting agitation rate between $200-2000 \,\text{rpm}$. The standard deviation is less than 35% of the mean value over



Figure 2. ESEM image of UF microcapsules containing DCPD core. The microcapsules were prepared following the procedure in figure 1 at 550 rpm agitation rate.



Figure 3. Mean microcapsule diameter vs agitation rate. Size analysis was performed by optical microscopy on data sets of at least 250 measurements at each agitation rate. Error bars correspond to 1 SD of the data. The solid line corresponds to a linear fit of the entire data on a log-log scale.

the entire range of diameters produced. Over the agitation rates investigated, the relationship between average diameter and agitation rate is linear in log–log scale, as is the dependence between droplet size and shear rate, as described by Taylor (1932). Although a logical correlation exists between agitation rate and shear rate, the connection to Taylor's work is further complicated because the fluid flow around the propeller is turbulent, rather than the laminar case analysed by Taylor (1932). Microeddies with a range of length scales are present in the flow, as described by Dobetti and Pantaleo (2002). In the region of flow away from the propeller, larger length scales dominate, leading to the major mode of the distribution shown in figure 4. Above a characteristic length scale, there are no microcapsules formed, a feature not represented by the normal curve. In the vicinity of the propeller blades, many smaller microeddies exist, resulting in a bias of the size distribution towards smaller length scales.

Microcapsule shell thickness

The surface morphology and shell wall thickness of microcapsules is investigated by electron microscopy. The microcapsule shell has a smooth inner membrane free of voids or inclusions and a rough porous morphology on the outer surface, as shown in figure 5. Excess ammonium chloride or resorcinol, addition of smaller volumes of DCPD, contaminated glassware, an unbalanced or unaligned mixer and lower initial pH all dramatically increase the thickness of the outer, permeable layer. Park *et al.* (2001) report that the presence of both a porous and non-porous zone is a common feature of UF microcapsules.

The shell wall thickness (of the smooth non-porous inner region) is largely independent of manufacturing parameters. Shell wall thickness consistently falls between 160–220 nm over the full range of microcapsule diameters investigated. Microcapsules in this range of shell thickness are sufficiently robust to survive



Figure 4. Microcapsule size distributions. At a 550 rpm agitation rate, the mean size is $183 \pm 42 \,\mu\text{m}$ ($\pm 1 \text{ SD}$). At 1800 rpm the mean size is $15 \pm 5 \,\mu\text{m}$. Standard normal distribution curves are overlaid with the data.



Figure 5. Microcapsule surface morphology. The rough outer surface is composed of UF nanoparticles (~150 nm) attached to the microcapsule shell.

handling and manufacture of self-healing polymers. When embedded in an epoxy matrix the microcapsules rupture and release their content at the site of damage (Brown *et al.* 2002). The rough porous structure on the outer surface is an agglomeration of UF nanoparticles, shown in figure 5.

Microcapsule surface morphology

The bath temperature, solution temperature and pH were monitored during a standard microencapsulation process (figure 6), while simultaneously removing aliquots from the emulsion bath at periodic intervals and quenching in 20 ml of cold (\sim 15°C) water. A sequence of aliquot images is shown along the bottom border of figure 6. Aliquots were imaged optically with incident light with black corresponding to an optically clear solution and white indicating a milky solution.



Figure 6. Temperature and pH profile during microencapsulation. Aliquot appearance was obtained by quenching in 15°C water at periodic intervals and imaging by reflected light.

Four distinct regimes are identified. In region I (0-50 min), the DCPD emulsion appears black (clear). At low agitation rates, individual DCPD droplets are observed. The DCPD rapidly coalesces to form a distinct second phase floating above the aqueous solution if agitation is stopped. During this time period, the bath temperature continuously increases to the set point, the solution temperature lags several minutes behind the bath temperature and the pH reduces from 3.50 to \sim 2.35. Region II (50–70 min) is defined by the transition to a cloudy emulsion and an associated slight increase in pH. Droplets remain as distinct microcapsules if agitation is stopped. However, the microcapsules clump and are too fragile to isolate. Region III (70-160 min) shows a transition to milky white emulsion in which the temperature stabilizes and the pH peaks at ~ 2.45 and then steadily decreases. Separable microcapsules appear when agitation is stopped. The microcapsule shell reaches its maximum thickness and the surface morphology transitions from smooth to rough in this region, as shown in figure 7. The milky white appearance of aliquot samples directly correlates to the development of UF nanoparticles in suspension. Electron micrographs of UF nanoparticles filtered from the solution and those found in the rough porous outer surface of microcapsules are indistinguishable. A stable pH is reached in region IV (160-240 min) and the suspension becomes clear with easily separated microcapsules.

The onset of rough surface morphology occurs \sim 75 min into the microencapsulation reaction. To preserve the smooth surface morphology, attempts were made to end the reaction at this time. If agitation is stopped and the reaction is allowed to cool naturally under ambient conditions, the emulsion forms a single gelatinous structure and individual microcapsules cannot be obtained. If agitation is stopped and the reaction is quenched with \sim 15°C water, individual smooth microcapsules are produced, but their quality is poor. The microcapsules are difficult to filter and, once separated, they turn yellow over a period of 3–10 days as the DCPD diffuses through the shell.



Figure 7. Microcapsule surface morphology evolution during Region III.

During *in situ* polymerization, the urea and formaldehyde react in the water phase to form a low molecular weight pre-polymer. As the molecular weight of the pre-polymer increases, it deposits at the DCPD-water interface. The UF ultimately becomes highly cross-linked and forms the microcapsule shell wall (Thies 1987). Gelation of bulk UF resin is attributed to the coalescence of a lyophobic colloidal sol (Pratt *et al.* 1985), which is known to precipitate out of solution as the molecular weight increases (Dunker *et al.* 1986). In light of this, the smooth non-porous microcapsule wall is believed to be the result of the deposition of low molecular weight pre-polymer at the DCPD-water interface, while the pre-polymer remains soluble. The formation of UF nanoparticles is attributed to precipitation of higher molecular weight pre-polymer in the aqueous solution and their aggregation and deposition on the capsule surface results in the rough, porous outer layer of the UF shell.

The appearance of UF nanoparticles in the emulsion and their subsequent deposition on the microcapsule surface occurs during Region III after the pH has dropped dramatically from initial conditions. Since the addition phase of UF polymerization is catalyzed by either acid or base, the precipitous drop in pH leads to a rapid increase in polymerization rate. Mehdiabadi *et al.* (1998) show that, as the pH decreases, the rate of increase in viscosity is accelerated dramatically. These rapid changes in viscosity at the DCPD–water interface affect the mechanics of droplet formation and suspension in shear flow. Sanghvi and Nairn (1992) conclude that interfacial surface tension was the dominant factor in controlling surface morphology of emulsion type microcapsules. Alexandridou *et al.* (2001) also report that surface morphology is dependent on functionality of the reactants and pH of the reaction solution.

Although acceptable levels of surface roughness for self-healing applications were obtained by the standard microencapsulation process, two modified processes were also investigated in an attempt to control surface morphology. First, microencapsulation was carried out at constant pH conditions (figure 8) by drop-wise addition of NaOH and HCl. Aliquot analysis of Region III reveals a milky white emulsion with separable microcapsules. However, the UF nanoparticles remained in suspension and did not deposit onto the microcapsule surface. The presence of suspended nanoparticles made the filtration process cumbersome and yields were low (< 10%). As shown in figure 9(*a*), the microcapsules produced by this method possessed a smooth surface morphology, free of nanoparticle agglomeration.

Surface roughness also decreased as the agitation rate increased. For a fixed volume of encapsulated DCPD, increasing the agitation rate reduced the mean microcapsule diameter and increased the DCPD–water interfacial area. To further investigate the effect of interfacial area for a fixed size of microcapsule, the volume of DCPD added to the emulsion was increased from 60 to 180 ml, while maintaining the same agitation rate of 550 rpm. As shown in figure 10, the emulsion transitioned directly to a clear suspension of distinct, easily filtered microcapsules in region III. The formation of UF nanoparticles was inhibited and the resulting



Figure 8. Temperature and pH profile during microencapsulation while maintaining constant pH conditions.







Figure 10. Temperature and pH profile during microencapsulation for increased interfacial area condition. The volume of DCPD encapsulated was increased from 60–180 ml, while maintaining 550 rpm agitation rate.

microcapsules had smooth surface morphology (figure 9(b)). The microcapsules were free flowing and yields were high (>85%).

Microcapsule fill content

Elemental analysis was performed on microcapsules to determine their fill content. Immediately following manufacturing and drying, microcapsules contain 83–92 wt% DCPD and 6–12 wt% UF, as measured by CHN analysis. The unidentified weight was accounted for by water absorption and UF chemical structure variation (Rammon *et al.* 1986). After 30 days exposed to ambient laboratory conditions, the average fill content decreased by 2.3 wt%. When used for self-healing epoxy, microcapsules are embedded in the matrix well within this

time frame. The surrounding matrix also limits further diffusion of DCPD through the microcapsule shell.

Conclusions

A process for the microencapsulation of dicyclopentadiene (DCPD) by *in situ* polymerization of urea-formaldehyde (UF) in an oil-in-water emulsion was developed to fulfil requirements for self-healing material applications. Microcapsules with average diameter in the range of $10-1000\,\mu\text{m}$ were manufactured by varying the rate of agitation over the range 200–2000 rpm. As the agitation rate increased, the mean diameter decreased. Spherical microcapsules were obtained in the form of a free flowing powder, exhibiting no agglomeration and yields of the preparation were high. Microcapsule shell thickness was 160-220 nm, providing excellent storage and release properties for self-healing applications. During the microencapsulation process, UF nanoparticles formed and deposited on the microcapsule surface producing a rough surface morphology. Surface roughness enhanced mechanical adhesion of the microcapsules when embedded in a polymer and improved performance in self-healing applications. The UF nanoparticles were prevented from depositing on the microcapsule surface by carrying out the reaction under constant pH conditions, but yields were low. Increasing the corewater interfacial area produced microcapsules with smooth surface morphology with high yields. Fill content was 83-92 wt% and remained high for the time period required for manufacture of self-healing polymers and polymer composites.

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